

Can Carbonaceous Particle Amendments—Including Biochar—Improve the Anaerobic Digestion of Agricultural Wastes?



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Anaerobic digestion can provide an environmentally sound approach to animal waste management

Open-air, swine lagoons

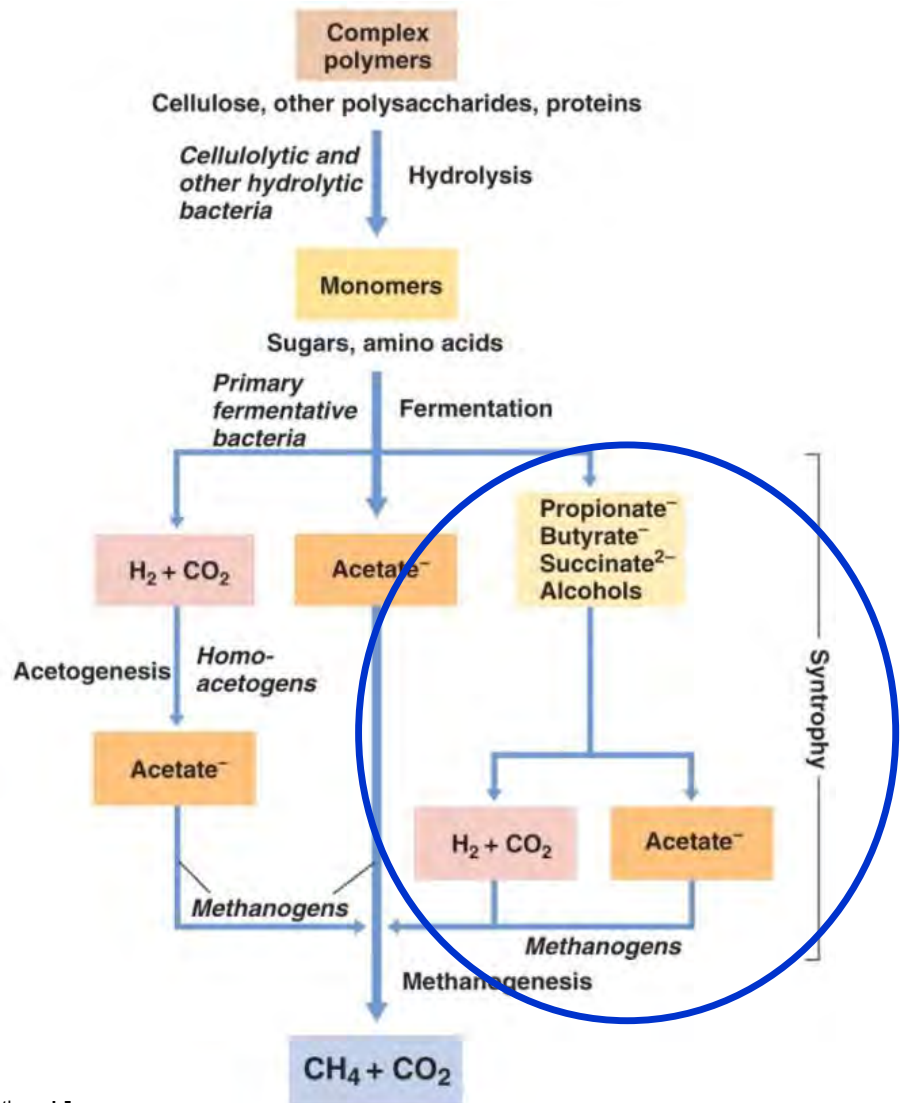


Anaerobic digesters

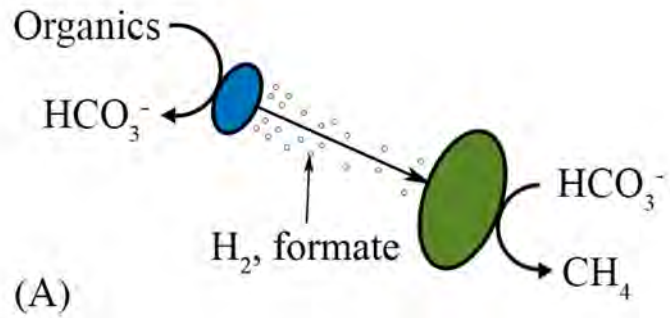


Anaerobic digesters face startup, stability, and economic challenges

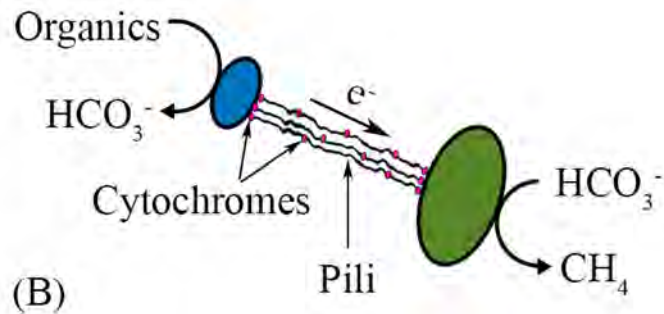
Efficient electron transfer within anaerobic communities is critical for stable anaerobic digester operation



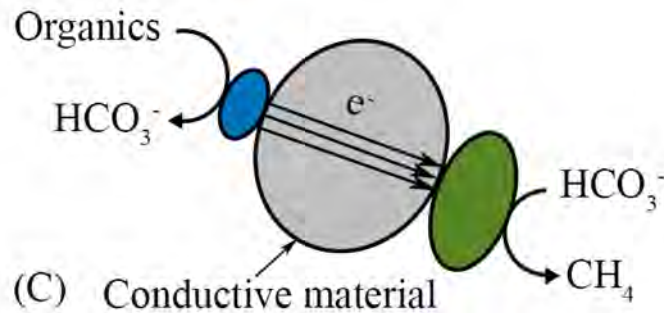
Microbe-to-microbe electron transfer mechanisms



Mediated interspecies electron transfer (MIET)



Direct interspecies electron transfer (DIET)

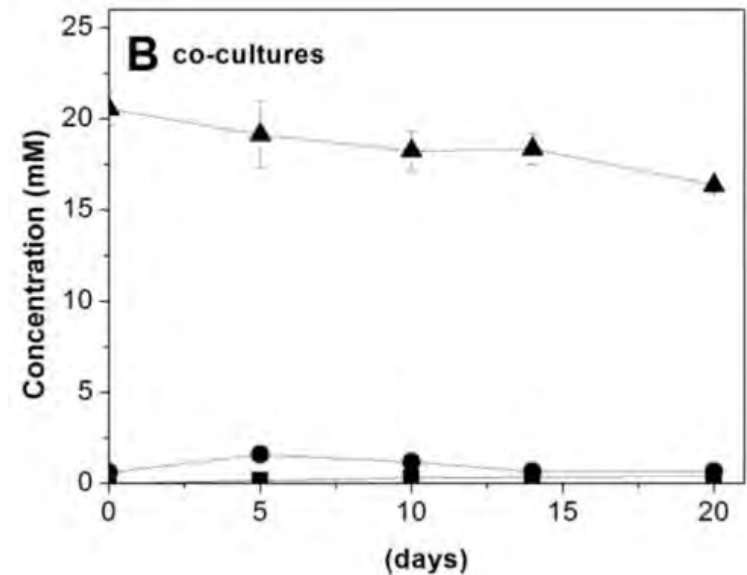
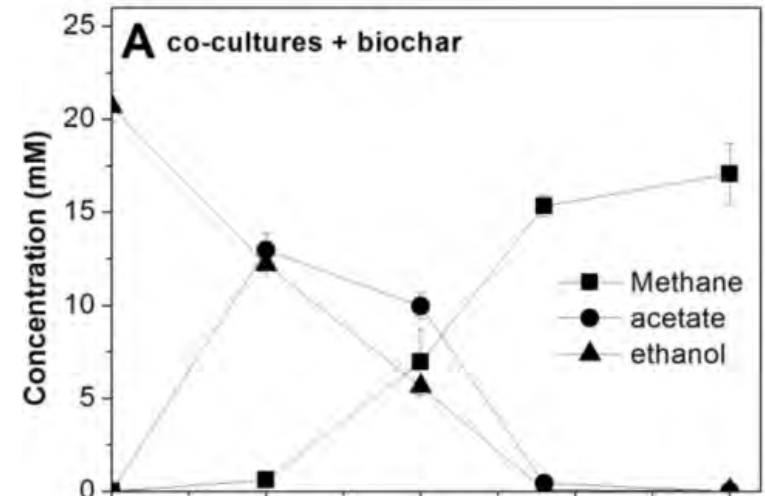
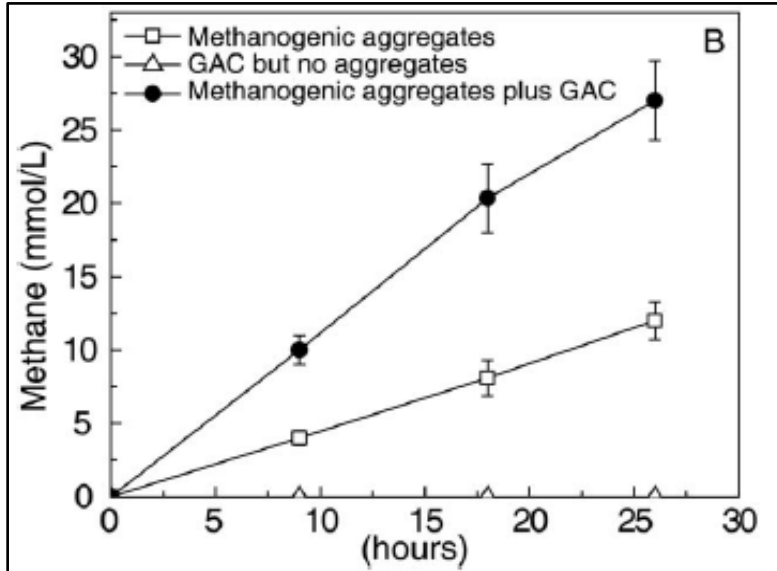


DIET via pyrogenic carbonaceous material (PCM)

Our understanding of DIET is primarily limited to defined cultures

Defined cultures

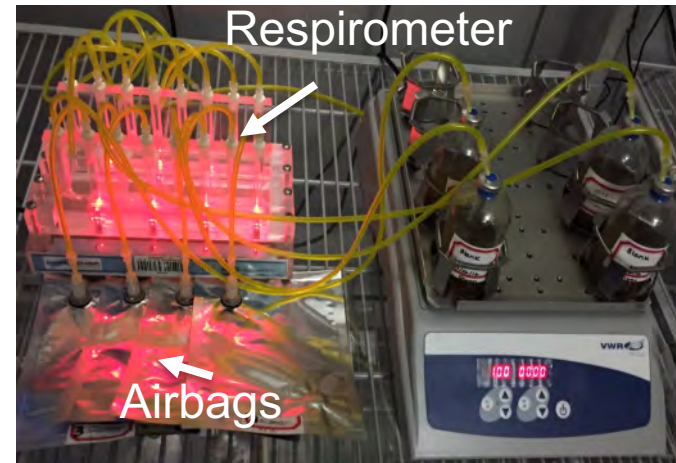
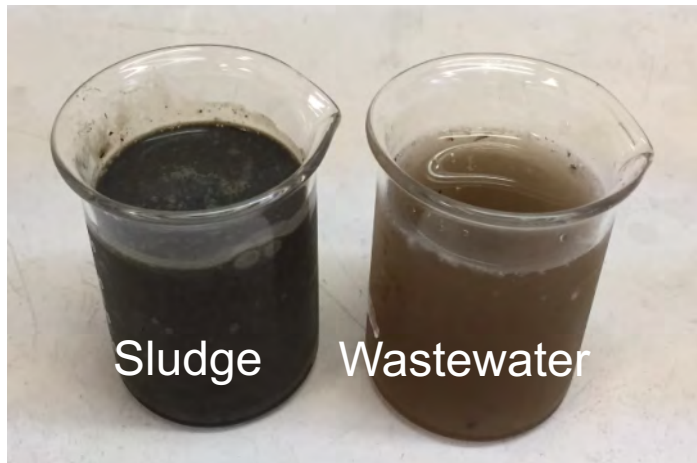
- *Geobacter metallireducens* and *Methanosarcina barkeri*
- *Geobacter metallireducens* and *Methanosaeta harundinacea*



Objective: To determine the impact of PCM addition on the anaerobic digestion of animal wastewater

Swine wastewater properties

Parameter	Unit	Values
Total chemical oxygen demand (TCOD)	mg/L	4,800 ± 1,700
Total suspended solids (TSS)	mg/L	7,100 ± 600
Volatile suspended solids (VSS)	mg/L	4,700 ± 800
pH		7.4 ± 0.2

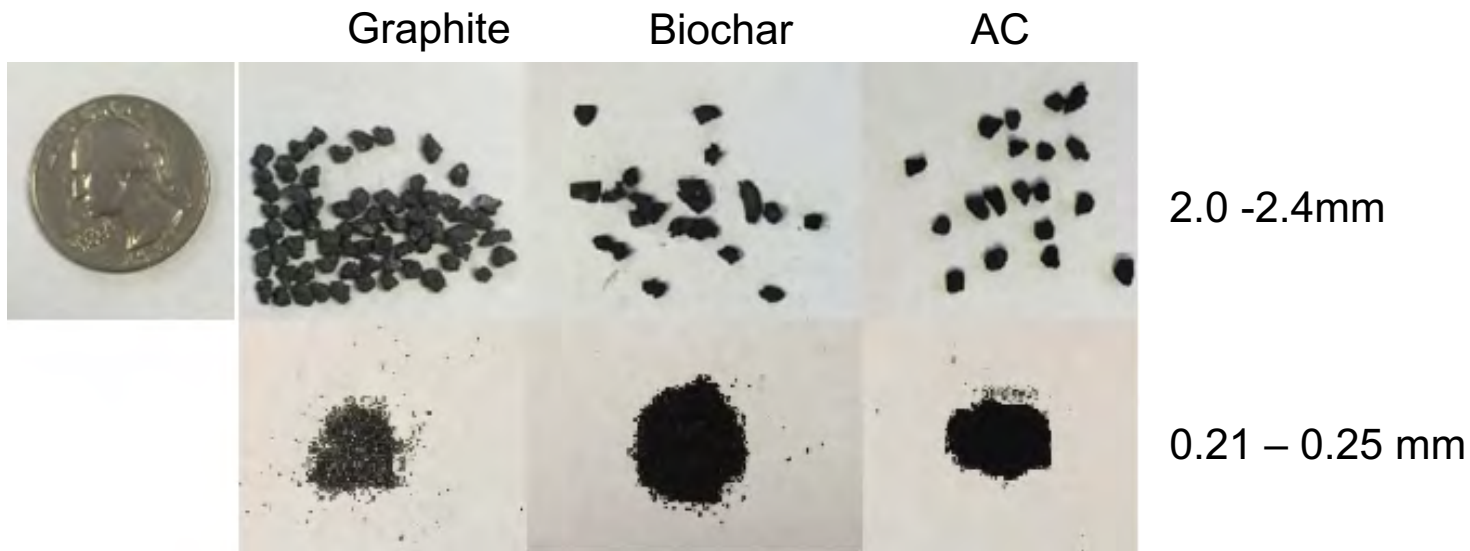


Particle properties

	Unit	Graphite	Biochar	AC
Conductivity	S/cm	17 ± 2.6	0.22 ± 0.046	1.2 ± 0.25
Surface area	m ² /g	0.6 - 19	15 - 209	258 – 1,596
Size	mm	2.0 - 2.4 (granule), 0.21-0.25 (powder)		
Loading	g particles /g VSS	6, 3, 1.5		

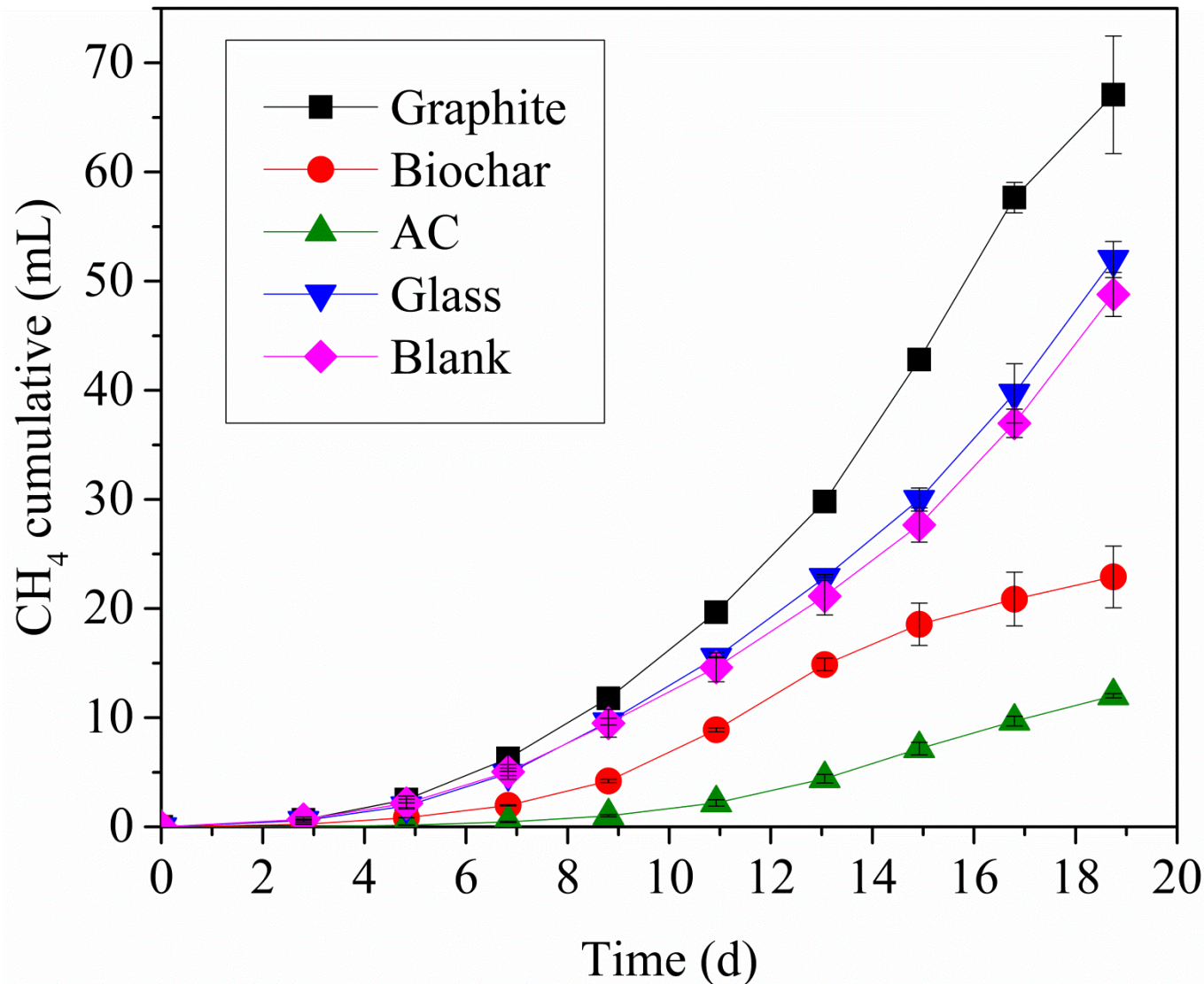
Controls

Blanks (no particles)
Glass particles



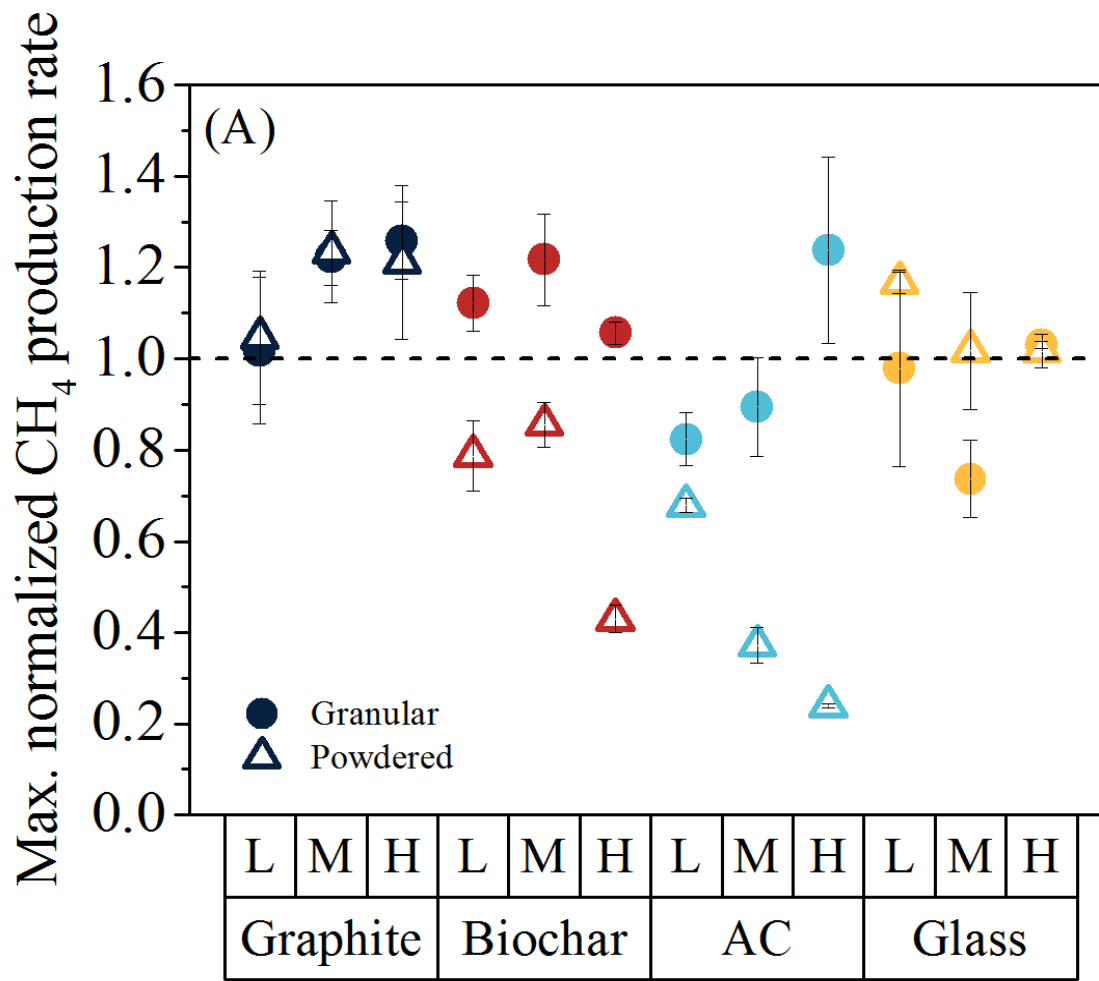
(Pierson H. O., Noyes Publications, 1993; Trammell M.P. & Pappano, P.J., Oak Ridge National Laboratory, 2011. Chen S. et al., *Sci. Rep.*, 2014; Ao G. et al., *Carbon lett.*, 2008; E. Berl, *Trans. Faraday Soc.*, 1938; Kastening B. et al., *Electrochim. Acta*, 1997; Shornikova O. N. et al., *Russ. J. Phys. Chem. A.*, 2009; Mishima D. et al., In *Electrical Insulation and Dielectric Phenomena*, 2011)

CH₄ generation rates were recorded in real-time to determine differences in bioreactor kinetics



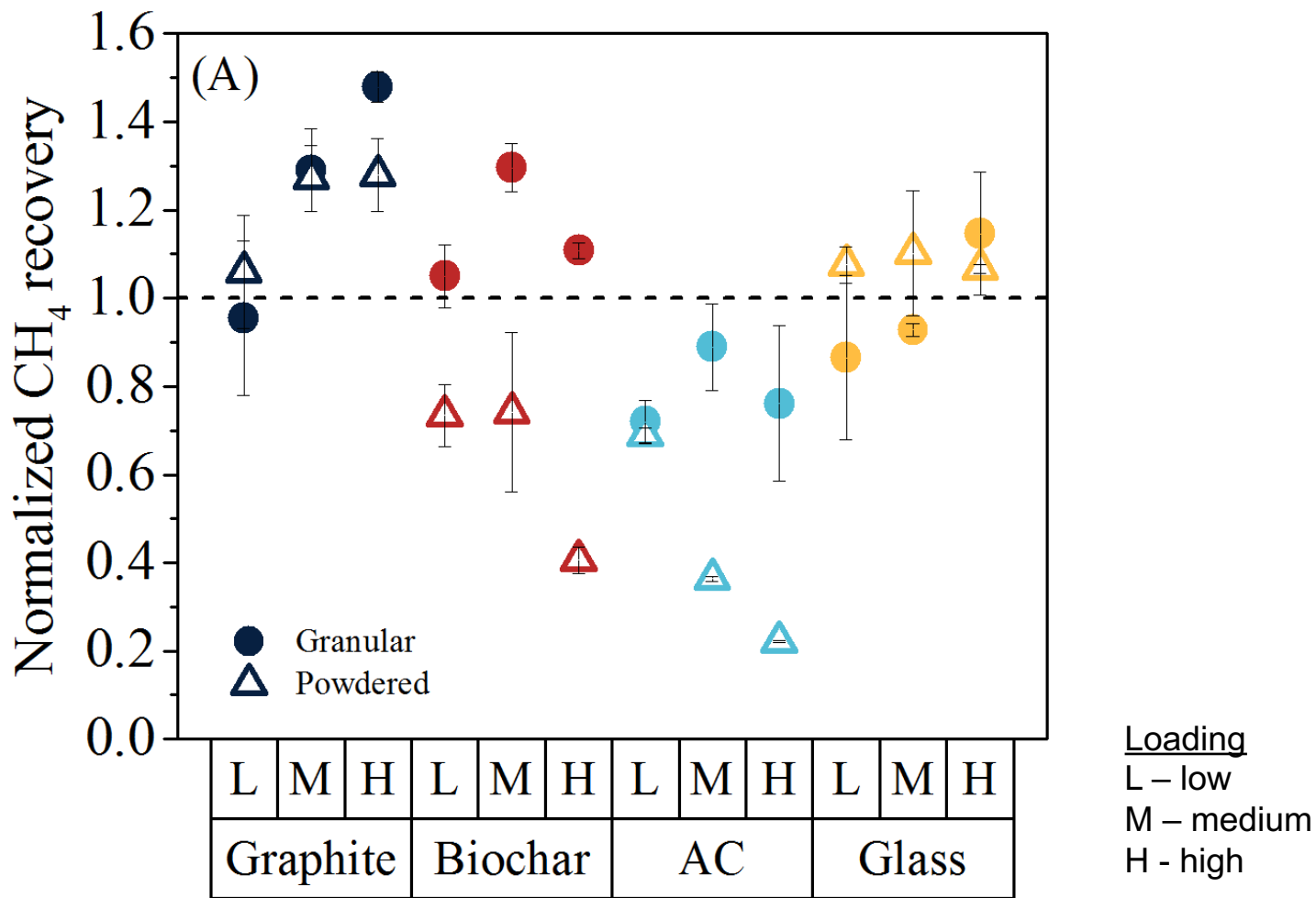
Sample cycle
particle size:
212-250 μ m,
loading rate:
6 g-particles/g-VSS

Graphite consistently resulted in higher normalized CH₄ production rates. Biochar & AC results depended on particle size



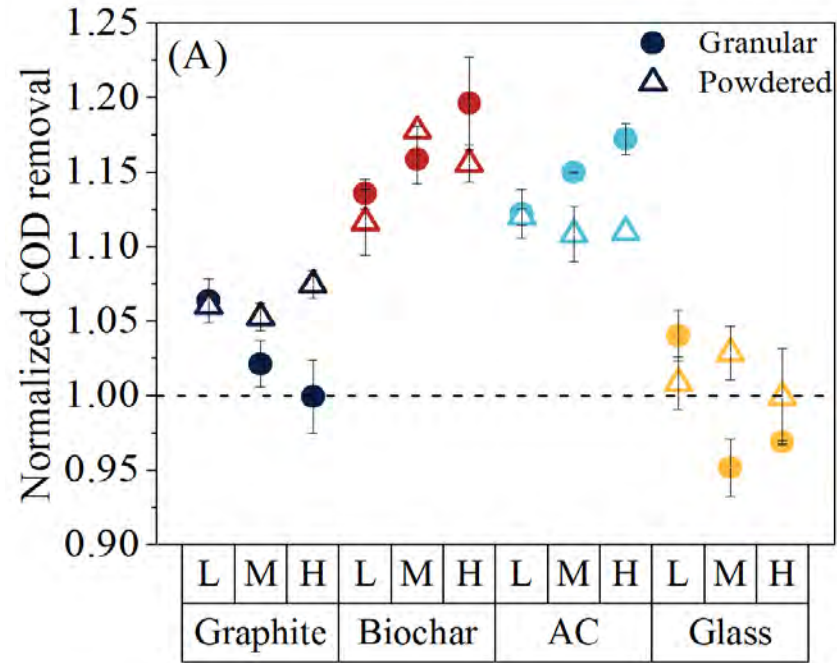
Loading
 L – low
 M – medium
 H - high

CH₄ recoveries followed a similar trend, except that all AC amendments decreased CH₄ recovery relative to the control

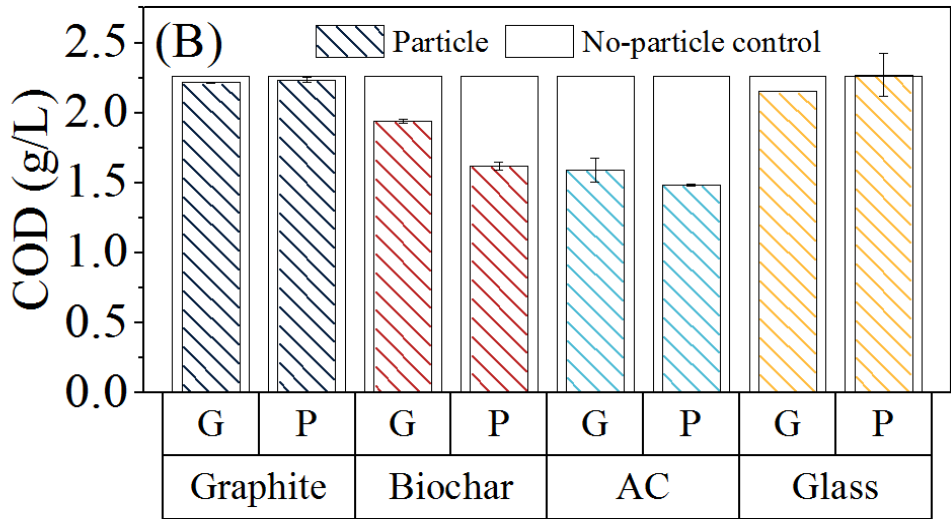


Although CH₄ recoveries were lower with biochar and AC, more COD was removed than the no-particle controls.

COD removal in bioreactors

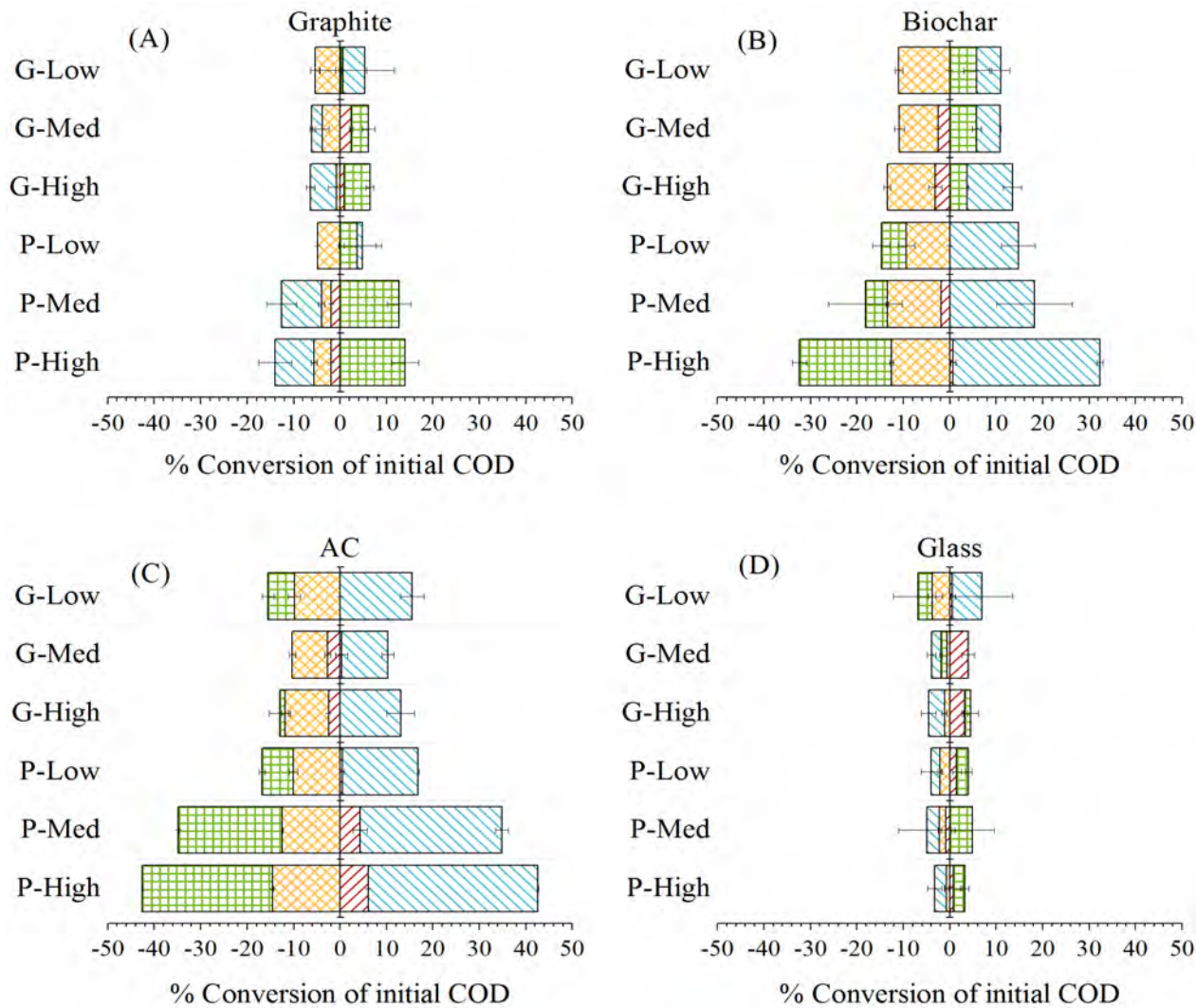


COD removal in sterile bioreactors

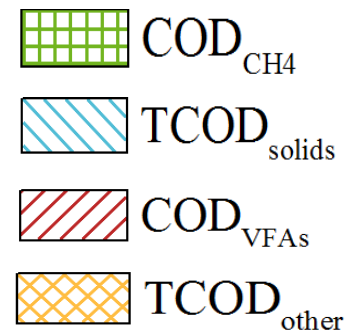


COD – chemical oxygen demand

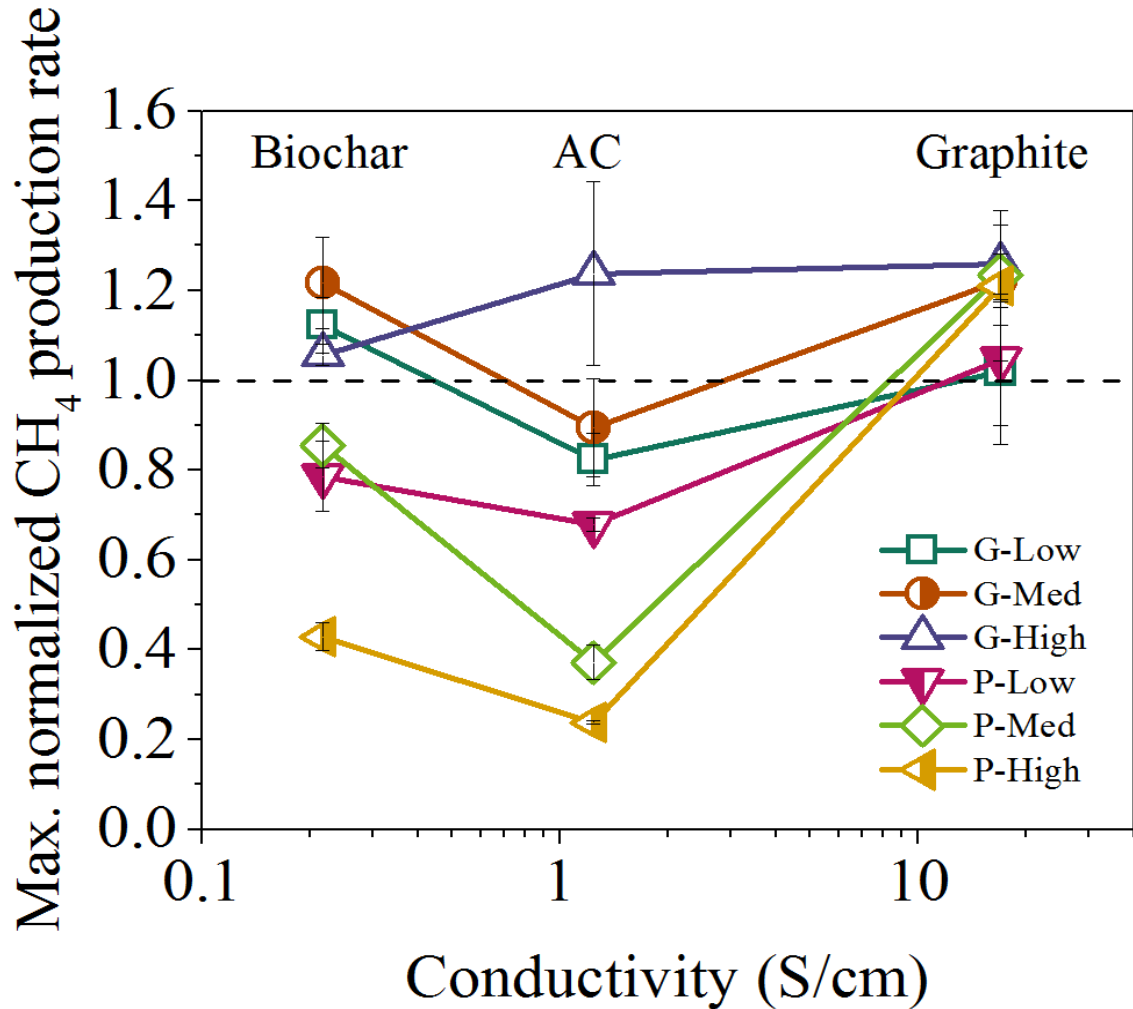
COD likely adsorbed to biochar and AC, which reduced its conversion to CH₄



Fate of initial COD:

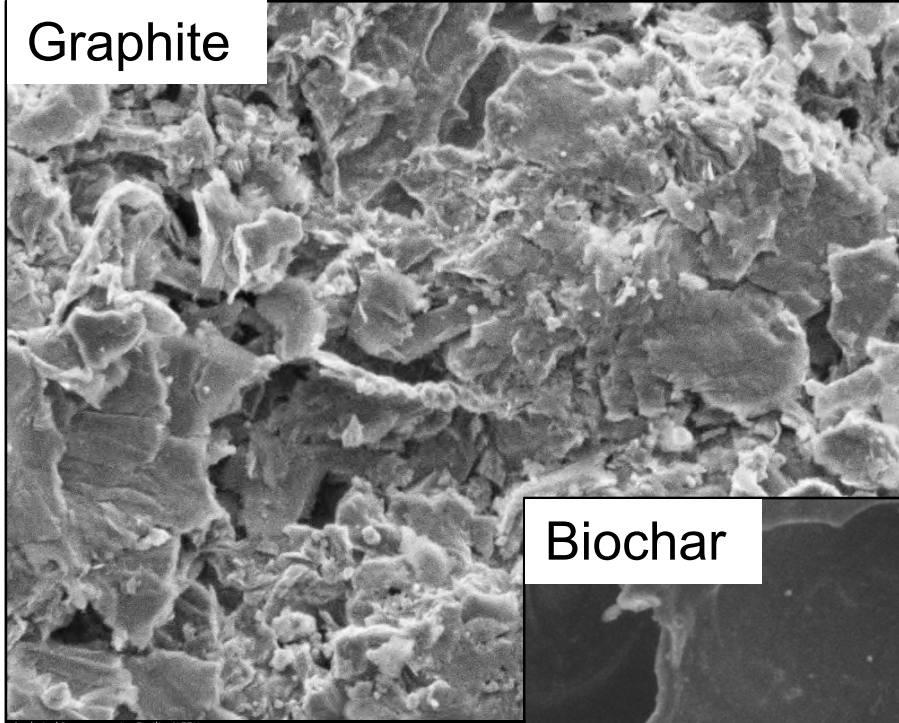


There were no clear relationships between CH₄ production and PCM electrical conductivity



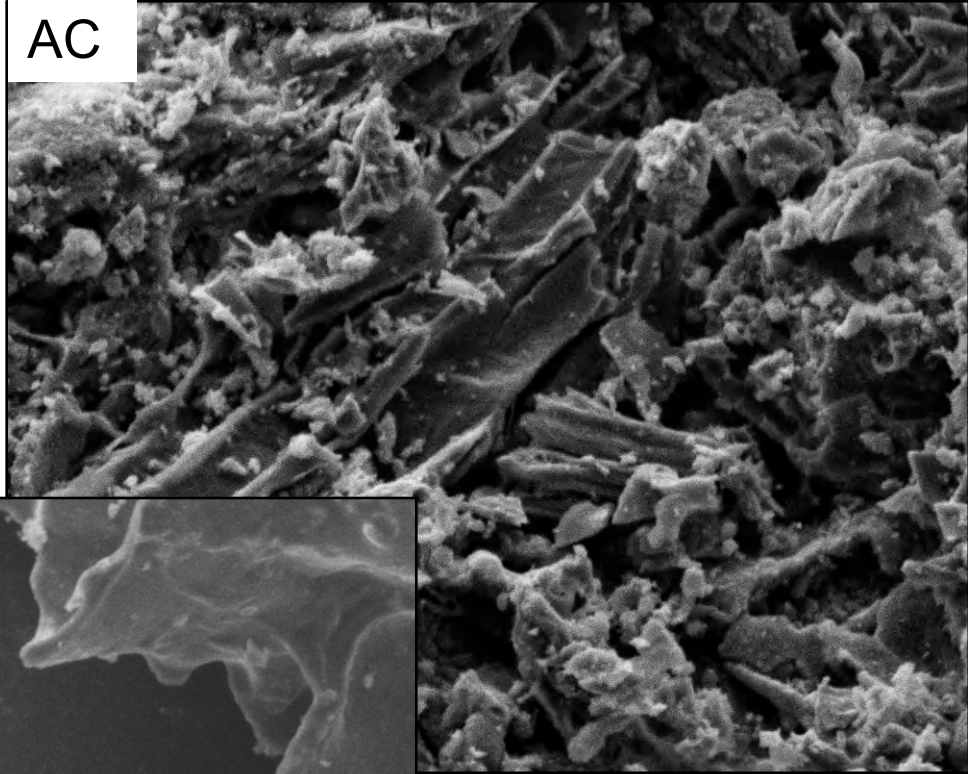
Surface property structures varied across all particle types

Graphite



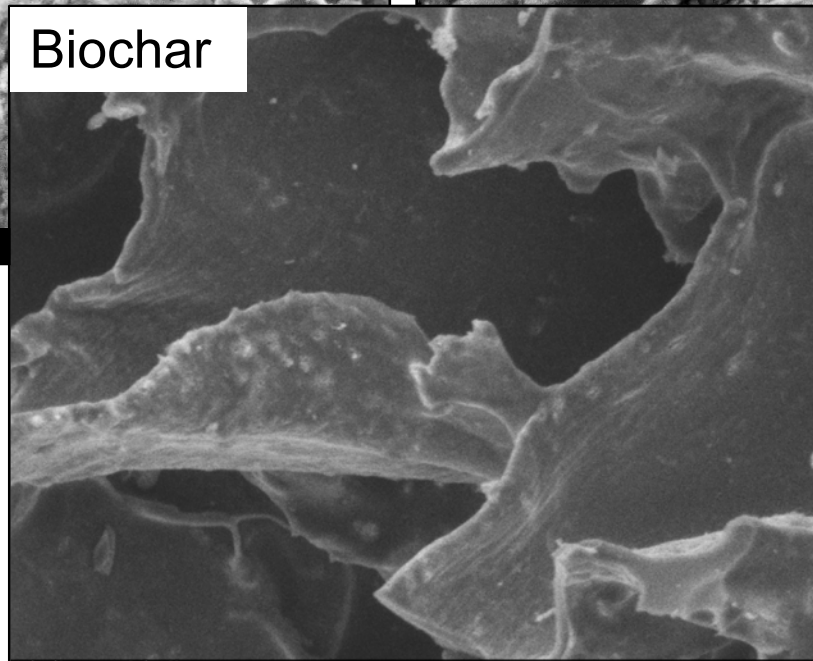
Analytical Instrumentation Facility NCSU
5.0 KV EM Mag 2500X

AC



10µm

Biochar



Analytical Instrumentation Facility NCSU
5.0 KV EM Mag 2500X

10µm

Overall, only graphite consistently yielded larger normalized CH₄ generation rates and recoveries

- Biochar was not far behind graphite, with granular biochar yielding > 20% increase in CH₄ production rates than bioreactors without particles.
- Powdered biochar and AC amendments led to a sharp drop in CH₄ production rates
- Adsorption was the likely cause of high COD removals and low CH₄ recoveries for biochar and AC
- Economics
 - Graphite: \$100 - \$2,000 / ton **\$3.36 / m³-wastewater**
 - AC: \$40 - \$4,000 / ton **\$1.34 / m³-wastewater**
 - Biochar: \$0.5 - \$800 / ton **\$0.02 / m³-wastewater**
- We still need a better understanding of what exactly happens when biochar is added to digesters

Acknowledgements

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Collaborator: Dr. Francis de Los Reyes

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